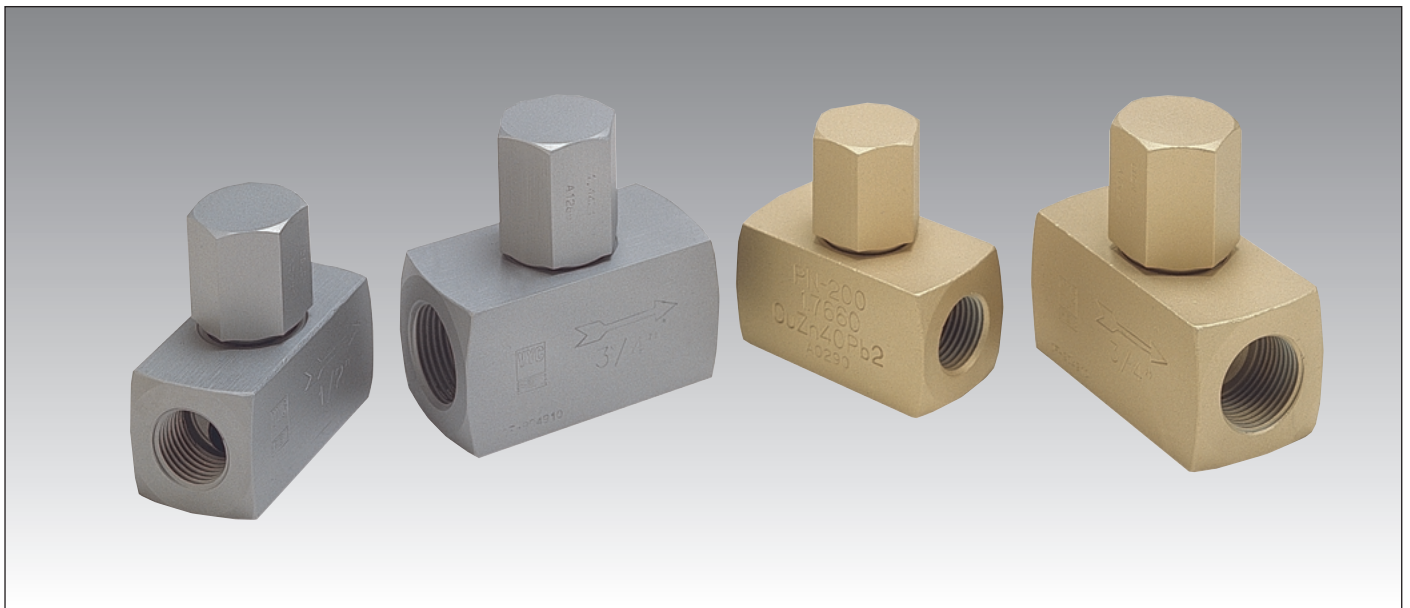


# Piston check valve

Model 179



For liquids, gases and steam.

For use in hydraulic, pneumatic, heating and steam systems, chemical and food industries, etc.

## Specifications

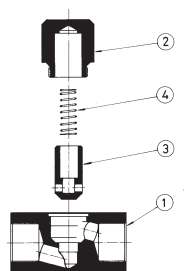
- Spring operated piston closure.
- Reduced pitch.
- Avoids ram shock when closing at zero pressure, remaining completely watertight at the time of fluid reversion.
- Highly tightness, exceeding the requirements of DIN-3230. Page 3.
- Easily assembled in any position in accordance with the direction of the fluid flow. Without spring only for horizontal mounting.
- Fully constructed from laminated bars.

## IMPORTANT

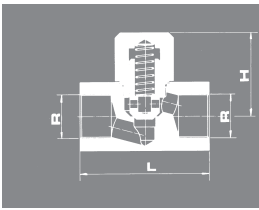
Depending on demand:

- Possibility of manufacture in other types of material, for use in special working conditions (high temperatures, fluids, etc.).
- Other connections.
- O-ring gasket closure.

N°. PIECE	PIECE	MATERIAL										
		BRASS			CARBON STEEL				STAINLESS STEEL			
1	Body	Brass (DIN-1.7660 CuZn40Pb2)			C. steel (DIN-1.1191 Ck-45)				S. steel (DIN-1.4401) (AISI-316)			
2	Cap	Brass (DIN-1.7660 CuZn40Pb2)			C. steel (DIN-1.1191 Ck-45)				S. steel (DIN-1.4401) (AISI-316)			
3	Piston	S. steel (DIN-1.4401) (AISI-316)			S. steel (DIN-1.4401) (AISI-316)				S. steel (DIN-1.4401) (AISI-316)			
4	Spring	S. steel (DIN-1.4571) (AISI-316Ti)			S. steel (DIN-1.4571) (AISI-316Ti)				S. steel (DIN-1.4571) (AISI-316Ti)			
DN		1/4" to 2" (GAS, NPT or SW)										
PN		200			250				250			
OPERATING CONDITIONS	PRESSURE IN bar	200	175	34	250	211	180	167	250	207	170	164
	MAXIMUM TEMP. IN °C	120	150	200	120	300	350(1)	400(1)	120	200	350(1)	400(1)
	MINIMUM TEMP. IN °C	- 60			- 10				- 60			



(1) For temperatures exceeding 300°C without spring only or depending on demand, with special spring.



R		1/4"	3/8"	1/2"	3/4"	1"	1 1/4"	1 1/2"	2"		
CONNECTIONS		Whitworth gas-tight cylindrical female thread ISO 228/1 1978 (DIN-259)									
		NPT thread ANSI - B 2.1									
		Socket welding ends SW ANSI - B 16.11									
H		34	39	48	55	62	64	82	85		
L		50	55	65	75	90	95	100	112		
REDUCED PITCH Ø		6,00	8,00	9,50	11,50	15,00	17,00	21,00	25,00		
WEIGHT IN Kgs.	BRASS	0,31	0,47	0,92	0,95	2,21	2,66	3,82	6,43		
	CARBON STEEL	0,29	0,44	0,78	0,88	2,05	2,47	3,56	6,16		
	STAINLESS STEEL	0,29	0,44	0,79	0,90	2,07	2,50	3,61	6,24		
CODE	BRASS	GAS	0041	0381	0021	0341	0101	0141	0121	0201	
		2003-179.	NTP	00411	03811	00211	03411	01011	01411	01211	
	CARBON STEEL	GAS	0044	0384	0024	0344	0104	0144	0124	0204	
		2003-179.	NTP	00441	03841	00241	03441	01041	01441	01241	02041
		SW	00442	03842	00242	03442	01042	01442	01242	02042	
	STAINLESS STEEL	GAS	0042	0382	0022	0342	0102	0142	0122	0202	
		2003-179.	NTP	00421	03821	00221	03421	01021	01421	01221	02021
		SW	00422	03822	00222	03422	01022	01422	01222	02022	

	OPENING PRESSURE IN mbar	FLOW COEFFICIENT								
						Kv m³/h ΔP = 1 bar	Cv l/min. ΔP = 1 Psi = 0,07 bar			
		WITHOUT SPRING	WITH SPRING			WITH SPRING	WITHOUT SPRING	WITH SPRING		
DIRECTION OF FLUID FLOW										
DN	1/4"	34,10	49,60	79,10	10,90	0,68	1,98	1,32	—	2,65
	3/8"	35,50	51,00	81,50	10,50	1,10	2,76	2,22	—	4,20
	1/2"	34,80	51,00	80,80	11,20	2,10	6,95	4,53	—	8,90
	3/4"	32,80	44,00	76,80	10,20	4,10	11,76	9,06	—	16,70
	1"	34,60	54,10	80,40	11,20	6,20	16,80	13,20	—	25,80
	1 1/4"	34,80	55,40	86,90	11,10	9,80	33,00	21,90	—	40,80
	1 1/2"	35,00	55,90	82,00	11,00	12,90	44,00	21,50	—	52,20
	2"	34,00	56,00	76,10	10,40	19,40	58,20	45,90	—	71,50

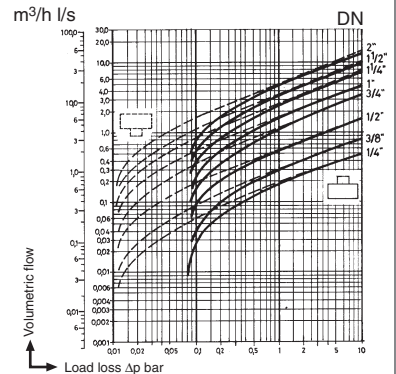
- (1) For other mounting positions, with or without spring, the flow coefficient varies by ± 2%.  
 (2) Flow coefficient for orientation. The volumetric flows which cause loss of pressure to 0,07 bar = 1 Psi are in unstable areas (See diagram of pressure loss).  
 (3) Opening pressures are greater than 0,007 bar = 1 Psi. The Cv coefficient cannot be determined.

### Load losses

The adjoining diagram reflects the load loss curves for water at 20°C. Values are based on valves without springs and installed horizontally. In order to determine other fluids load losses, calculate the flow of these equivalent to water.

$$Q_A = \sqrt{\frac{\rho}{1.000}} \cdot Q$$

- $Q_A$  = Flow equivalent to water in m³/h.  
 $\rho$  = Fluid density in operating conditions in Kg/m³.  
 $Q$  = Fluid flow in operating conditions in m³/h.



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